

Utilization of Hydroxyapatite from Quail Eggshells as an Adsorbent for Lead Metal Ions Pb(II)

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Abstract

Lead is a toxic metal known for its harmful effects, even in minor quantities, because it does not break down naturally and can therefore pollute ecosystems. This research involved the creation of hydroxyapatite using quail egg shell through a sol-gel method, which served as a medium for capturing Pb ions in a batch process by assessing different parameters. The created material was analyzed using X-Ray Diffraction (XRD) to confirm its crystal form, SEM (Scanning Electron Microscopy) to analyze its surface, FTIR (Fourier Transform Infrared Spectroscopy), and morphology to determine the functional units that were present. Sorption tests were performed under various scenarios, encompassing different pH levels, the initial Pb ion concentration, and time of contact, with the outcome evaluated through atomic absorption spectrophotometry (AAS). The results demonstrated that the optimal conditions for Pb ion uptake were observed at a concentration of 800 mg/L with 0.1 g of adsorbent as well as a contact time of 60 minutes, achieving a lead ion removal rate of 71.48%. The sorption isotherm followed the Langmuir model, while the sorption kinetics fit the pseudo-order two model, indicating a monolayer sorption mechanism on a uniform surface. These outcomes suggest hydroxyapatite derived from quail eggshells is a promising eco-friendly material for treating wastewater containing heavy metal ions.

Keywords

Hydroxyapatite, Adsorption, Quail Eggshell, Lead Metal Pb(II)

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1. INTRODUCTION

Among the various contaminants often found in water, industrial effluents, heavy metals, and dyes play a significant role. These substances generally come from industrial activities such as mining, metal plating and smelting, the textile and dye industry, leather tanning, pesticide production and fermenters, papermaking, and the paint industry. Indiscriminate disposal of heavy metals and dyes beyond the prescribed limits can have serious impacts on health and become a major cause of environmental problems (Ame-naghawon et al., 2022). Toxic heavy metals like lead (Pb) are commonly present in water environments. As per the regulations established by the WHO (World Health Organization), the limited allowable concentration of lead (Pb) in water is 0.05 mg/L. Research shows that lead (Pb) exposure can cause brain disorders, cancer, anorexia, anemia, kidney damage, and dementia (Li et al., 2024). Multiple methods have been utilized to address these issues, as example flocculation, chemical precipitation, neutralization, ion exchange, adsorption, and membrane separation. Nev-

ertheless, numerous approaches encounter challenges like expensive equipment, complications in execution, generation of harmful sludge, and significant operational expenses. On the contrary, adsorption stands out as a cost-effective, the most straightforward, eco-friendly, easy-to-execute, as well as efficient solution (Kotnala et al., 2024).

Commonly utilized materials for extracting heavy metals consist of activated carbon, zeolites, chitosan, ion exchange resins, industrial solid waste, and hydroxyapatite (Yan et al., 2014). The implementation of hydroxyapatite in the extraction of heavy metals has garnered significant attention from researchers, mainly due to its plentiful availability, eco-friendly characteristics, and ion exchange capabilities. The presence of calcium ions (Ca^{2+}), phosphate ions (PO_4^{3-}), and hydroxyl ions (OH^-) ions makes HAp have both positive and negative surface charges, making it capable of bonding with various other atoms (Xu et al., 2023). Hydroxyapatite can be synthesized using calcium-based materials from natural materials such as limestone shells, eggshells, and green mussel shells (Alif et al., 2024). The potential for eggshell waste in Indonesia is quite large. One of them is

quail eggshell, which makes up approximately 10% of the egg's total weight and is often a waste from the egg processing industry and households, although it is sometimes used in small-scale applications. The primary elements of quail eggshell are calcium carbonate (over 95%) and protein, a viable alternative to calcium carbonate that can be efficiently obtained and utilized in the process of making hydroxyapatite (Vinayagam et al., 2023). The utilization of quail eggshells as a source of calcium in hydroxyapatite synthesis is an environmentally friendly process because it utilizes waste to prevent environmental pollution. The purpose of this investigation is to analyze the efficacy of hydroxyapatite derived from quail eggshells in absorbing lead metal ions (Pb), utilizing various factors assessed through XRD, SEM, and FTIR methods.

2. EXPERIMENTAL SECTION

2.1 Materials and Instruments

Quail eggshells were collected from Lima Puluh Kota District, West Sumatra, Indonesia. Diammonium phosphate ((NH₄)₂HPO₄), nitric acid (HNO₃), potassium nitrate (KNO₃), potassium hydroxide (NaOH), and Pb(NO₃) all produced by Merck, were used in this study. All analytical reagents were dissolved using distilled water (H₂O). The equipment used in this study consisted of mortar and pestle, thermo insight (furnace), analytical balance, hot plate, oven (Labtech), pH meter, magnetic stirrer, 200 mesh sieve (75 μm), burette, rotary shaker (Edmun Buhler 7400 Tubingen), and necessary laboratory glassware. Analysis and characterization of the adsorbents were performed by AAS (Shimadzu AA7000G, Autosampler), SEM-EDX (Carl Zeiss Scanning Electron Microscope With EDX EVO 10) and FTIR (PerkinElmer version 10.6.1).

2.2 Methods

2.2.1 Sample Preparation

The collected quail eggshells were washed using running water, then the shells were boiled for 30 minutes at 100°C to remove impurities and rinsed using distilled water. Next, the quail eggshells were oven-dried at 105°C for half an hour. The dried quail eggshells were reduced in size until they became powder. Furthermore, quail eggshell powder was sieved using a 200 mesh sieve (75 μm) which aims for size uniformity. Quail eggshell powder was calcined for 5 hours at 900°C using a furnace (Alif et al., 2018). The quail eggshell powder was then used in the hydroxyapatite synthesis process.

2.2.2 pHpzc (Point Zero Charge) Study

Adsorption experiments and point zero charges were performed by combining the adsorbent (0.1 g) with 0.1 M KNO₃ (50 mL) across various pH levels. The concluding pH was assessed, and a graph was generated contrasting it with the starting pH. The intersection point of the curve that cuts through the zero marker on the X-axis represents the point

of zero charge or pHpzc (zero charge point). The variation in pH (ΔpH) at equilibrium was determined by applying the formula $\Delta\text{pH} = (\text{pH}_f - \text{pH}_i)$ (Hassan et al., 2020).

2.2.3 Adsorption Study

A total of 0.1 g of hydroxyapatite adsorbent was put into 50 mL of Pb(II) metal ion solution with solution pH 4. Then the concentration of the solution was adjusted with a concentration variation of 100 - 1000 mg/L. Then dishaker for 60 minutes at a speed of 200 rpm. After obtaining optimum absorption conditions at certain concentrations, experiments were then carried out to identify the ideal choice mass and contact time for the absorption of Pb(II) metal ions by hydroxyapatite. The mixture was subsequently strained, and the filtrate was measured by AAS (Putra et al., 2024). The sorption capability of Pb(II) metal ions was decided by applying Equation 1:

$$q = \frac{C_0 - C_e}{m} \times V \quad (1)$$

The proportion absorption of Pb(II) metal ions can be determined in Equation 2:

$$R = \frac{C_0 - C_e}{C_0} \times 100\% \quad (2)$$

The sorption capacity (q_e) of Pb(II) metal ions retained by the hydroxyapatite adsorbent (measured in mg/g) is determined using the primary (C₀) as well as last (C_e) concentrations of metal ions in the solution (mg/L), the solution volume (V) in liters, and the mass (g) of the adsorbent used in grams.

3. RESULTS AND DISCUSSION

3.1 pHpzc and Adsorption Studies

The pH point of zero charge, or pHpzc, plays an essential part in shaping the surface charge of an adsorbent. At this specific pH level, the total charge on the adsorbent becomes neutral, which occurs under specified conditions of temperature, pressure, and solution makeup. The pHpzc signifies that, at this pH, the total count of positive surface charges matches the total count of negative charges. Establishing the pHpzc has an impact on the adsorption percentage, which varies depending on the material in question (Al-Maliky et al., 2021). pHpzc of hydroxyapatite adsorbent is fully visible in Figure 1.

According to Figure 1, the determination of pHpzc is done by determining the intersection point between The initial pH curve as well as the last pH curve of the solution. Determination of pHpzc causes changes in the speciation of target adsorbate molecules, where if the pH of the target solution >pHpzc indicates that the adsorbent surface holds a full positive charge as a result of protonation, but if the pH of the target solution <pHpzc indicates that the adsorbent surface is negatively charged due to deprotonation

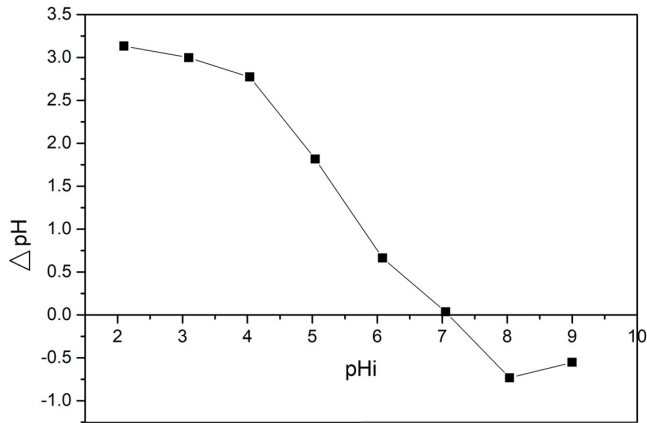


Figure 1. pH_{Pzc} Hydroxyapatite

(Adawiyah et al., 2024). Hydroxyapatite has a neutral charge at pH 7.05. When the pH is less than pH_{Pzc}, it causes hydroxyapatite to be positively charged so that it can be used in anionic absorption and vice versa (Zein et al., 2024). According to the evaluation of pH_{Pzc}, the impact of pH on the absorption of Pb(II) metal ions is carried out in the range of 3 - 8 obtaining optimal conditions at pH 4.

3.2 Effect of Concentration and Isotherm Evaluation

The goal of concentration assessment is to evaluate how the quantity of active sites present on the adsorbent's surface relates to the rise in solution concentration. The influence of solution concentration on the ability to absorb Pb(II) metal ions with hydroxyapatite as the adsorbent is illustrated in Figure 2.

Figure 2, shows that the concentration increases as the adsorbate concentration increases. The rise in the capacity for metal ion adsorption is attributed to multiple elements including the relationship between metallic surfaces and metal ions, the ability to diffuse, and the existence of functional sites on the surface of the adsorbent (Bilal et al., 2024). This phenomenon is evident as the concentration of the adsorbate rises from 100 mg/L to 800 mg/L, attributed to the active sites of hydroxyapatite that are capable of interacting with Pb(II) metal ions. The peak absorption concentration for Pb(II) metal ions was attained at 800 mg/L, showcasing an absorption capability of 285.93 mg/g as well as an absorption efficiency of 71.48 for Pb(II) metal ions. The optimal concentration indicates that there has been an equilibrium between the concentration of Pb(II) metal ions that have been absorbed with the hydroxyapatite adsorbent (Wang et al., 2018). After reaching the optimal concentration, the adsorption capability decreased at a concentration of 900 mg/L - 1000 mg/L because hydroxyapatite had reached the saturation point. The adsorption isotherm model aims to determine the interaction between Pb(II) metal ions in liquid and solid phases when reaching equilibrium to obtain

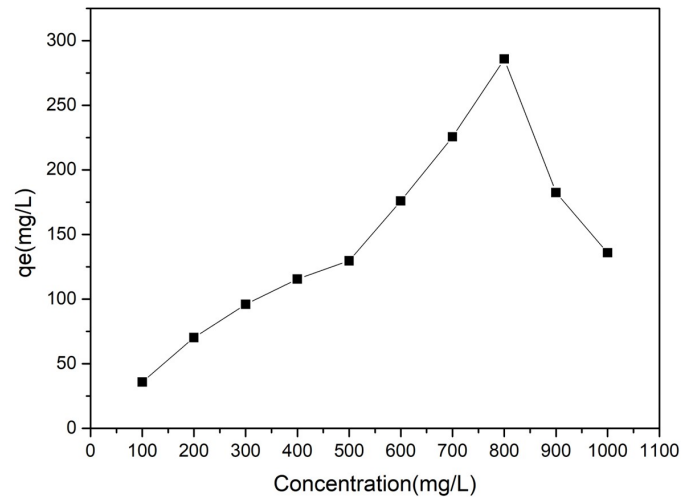


Figure 2. Impact of Initial Levels of Heavy Metals on the Adsorption Ability of Hydroxyapatite, Ideal pH (pH 4), Contact Duration 60 Minutes, Agitation Frequency 200 rpm, and Adsorbent Weight 0.1 g

the right correlation (Li et al., 2024). Langmuir Model can be determined Equation 3:

$$\frac{1}{q_e} = \frac{1}{k_l q_m C_e} + \frac{1}{q_m} \quad (3)$$

where q_e is the adsorption capacity (mg/g), c_e is the concentration (mg/L) at equilibrium, q_m is the maximum monolayer adsorption capacity (mg/g) and K_L is the Langmuir constant (L/mg). Freundlich Model can be determined by Equation 4:

$$\log q_e = \log K_f + \frac{1}{n} \log C_e \quad (4)$$

where K_f is the Freundlich constant (L/mg), and n is the adsorption strength. The adsorption isotherm model achieves balance by satisfying the Langmuir isotherm equation, exhibiting a maximum absorption capability of 285.93 mg/g. This suggests that the adsorption happens on a uniform surface containing similar binding sites, generating the creation of a single layer on the adsorbent's surface, known as monolayer adsorption (Zeng et al., 2018). The results from the curve indicate that the Langmuir isotherm model produced a linear equation represented by $y = 0.0094x + 0.0251$, illustrating the concept of the coefficient of determination (R^2) of 0.9445, which is near 1, along with a Langmuir constant (K_L) of 0.0539, as shown in Table 1. The Langmuir constant value (K_L) shows the attraction between the adsorbent and heavy metals, where the greater the equilibrium constant value, the greater the affinity of the adsorbent to metals (Trakoolwannachai et al., 2019). Table 1. Freundlich for the adsorption of Pb(II) as well as Parameters from Langmuir ions using hydroxyapatite.

Table 1. Langmuir and Freundlich Parameters Regarding the Sorption of Pb(II) Ions Utilizing Hydroxyapatite

Parameters	Langmuir			Freundlich			
Pb(II)	q_{max} (mg/g)	K_L (L/mg)	R_L	R^2	K_F (L/mg)	$1/n$	R^2
	273.9726	0.0539	0.0235	0.9228	97.6517	0.4913	0.619

3.3 Effect of Contact Time and Kinetics Study

The purpose of establishing contact time is to gather data regarding the shortest duration needed by hydroxyapatite to absorb Pb(II) metal ions. Based on collision theory, the reaction rate is influenced by the number of collisions in a unit of time. The more frequent collisions occur, the faster the reaction takes place until it reaches equilibrium conditions (Jaihan et al., 2022). Figure 3 highlights the significance of contact duration on the capacity to absorb Pb(II) metal ions.

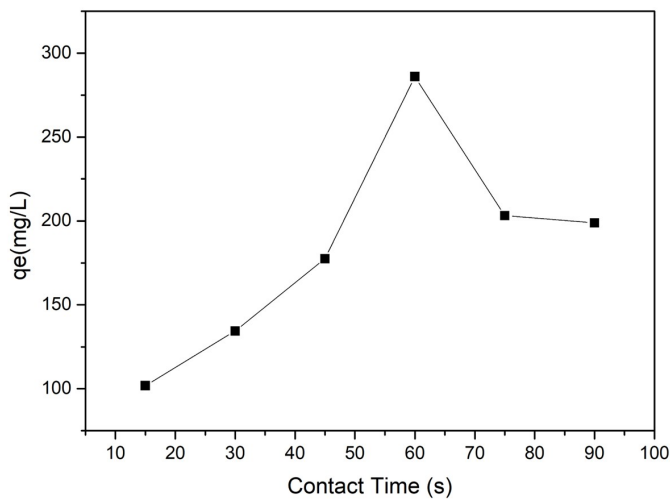


Figure 3. Impact of Initial Metal Weight Concentration on the Adsorption Capability of Hydroxyapatite; Ideal pH (pH 4), Concentration Set at 800 mg/L, Adsorbent Weight 0.1 g, and Agitation Frequency of 200 rpm

Figure 3 illustrates the rise in adsorption capacity from 15 minutes to 60 minutes of contact time. This is because the duration of the collision is extended between hydroxyapatite adsorbent and Pb(II) metal ions, the more Pb(II) metal ions are absorbed by hydroxyapatite adsorbent due to the more active groups on hydroxyapatite adsorbent that bind with Pb(II) metal ions (Wibiyan et al., 2024). The best duration for soaking to absorb Pb(II) metal ions was found to be 60 minutes, achieving an adsorption rate of 285.93 mg/g and a metal uptake efficiency for Pb(II) ions at 71.48%. After reaching equilibrium, the ability to adsorb declined due to the surface of the hydroxyapatite adsorbent was closed which caused the obstruction of Pb(II) lead ions to enter the openings of the hydroxyapatite adsorbent (Ali et al., 2016). The reaction kinetics are related to the functional groups

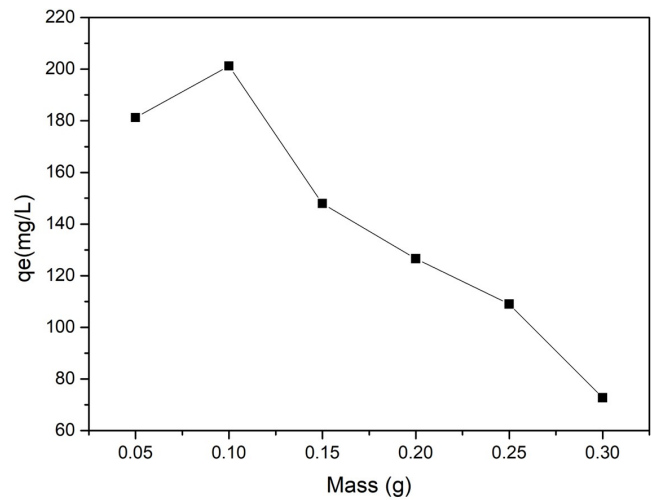


Figure 4. Influence of Adsorbent Weight on the Adsorption Ability for Pb(II) Metal; Ideal pH (pH 4), Concentration 800 mg/L, Contact Duration 60 Minutes, and Stirring Frequency of 200 rpm

and the concentration of adsorbate concentration (Putri et al., 2024). The pseudo-first-order model, the pseudo-second-order model, and the model of intraparticle diffusion sequence were employed to establish the mechanisms of adsorption and the kinetic constants involved in the elimination of heavy metals. The primary pseudo-kinetic model presumes the quantity of pores occupied by the solute is proportional to the adsorption rate (Zhou et al., 2023). The transformed version of the first-order pseudo-kinetic model presented can be determined in Equation 5:

$$\log(q_e - q_t) = \log q_e - \frac{k_1 t}{2.303} \quad (5)$$

where k_1 is the first-order reaction order rate constant, t is time (minutes), q_e is the adsorption capacity (mg/L) at equilibrium, and q_t is the amount adopted at a given time. While the second-order model can be determined in Equation 6:

$$\frac{t}{q_t} + \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (6)$$

k_2 manifests the constant of the second order, q_e is the adsorption capability (mg/L) at equilibrium, and q_t is the amount adopted at a given time. The adsorption kinetics model that occurs between hydroxyapatite and Pb(II)

metal ions tends to follow the second-order pseudo adsorption kinetics model (Table 2) which indicates that the reaction system that happens in the adsorption process occurs chemically. It is observable from the curve results that the second-order pseudo adsorption kinetics model obtained a linear equation $0.0037x + 0.0838$ with a coefficient of determination R^2 0.8221. The adsorption kinetics model tends to occur when the R^2 value is greater than the other adsorption kinetics models.

3.4 Effect of Adsorbent Mass

The objective of measuring mass is to enhance the ability of hydroxyapatite to adsorb Pb(II) metal ions during the absorption process. The influence of the mass of the hydroxyapatite adsorbent on its capacity to absorb Pb(II) ions is illustrated in Figure 4.

As displayed in Figure 4 the capacity for adsorption rises as the mass increases from 0.05 grams to 0.1 grams. This is due to the higher amount of adsorbent leading to an increased quantity of active sites available on the adsorbent's surface (Iconaru et al., 2018). The optimal mass of Pb(II) metal ion absorption was obtained at a mass of 0.1 gram capable of absorbing 285.93 mg/g and Pb(II) metal ion absorption efficiency of 71.48%. The optimal mass indicates that Pb(II) metal ions have been maximally absorbed by hydroxyapatite. After reaching the optimal mass there is a decrease in adsorption capacity from a mass of 0.15 grams - 0.3 grams. The reduction in absorption capability is caused by the solution of Pb(II) metal ions having reached the saturation point to bind with hydroxyapatite (Ramadhani et al., 2020). The more active sides that are not saturated during the adsorption process indicate that more active sides are available to bind between the adsorbent and the metal. The more adsorbent used, it will form coagulation which causes a decrease in the adsorbent's surface area in the process of metal ion absorption (Chaidir et al., 2015).

3.5 Adsorbent Characterization

Hydroxyapatite was analyzed through XRD (X-Ray Diffraction), FTIR (Fourier Transform Infrared), and SEM (Scanning Electron Microscopy) to provide information on the macromolecular structure as well as the chemical makeup of the adsorbent. Analysis using XRD aims to identify the crystal phase in hydroxyapatite. The results of the analysis in the form of a diffractogram that relates the 2θ angle to the peak intensity will then be compared with JCPDS Number 09-0432 data. The diffractogram of hydroxyapatite at 900°C (Figure 5) shows high intensity with most peaks reflecting the hydroxyapatite phase, namely at angles $2\theta = 16.63^\circ, 25.79^\circ, 31.51^\circ, 31.89^\circ, 32.66^\circ,$ and 33.99° . In addition, there are some low-intensity peaks at $2\theta = 18.54^\circ, 21.61^\circ, 39.81^\circ,$ and 42.10° .

Analysis using FT-IR seeks to recognize functional groups in the form of absorption peaks contained in hydroxyapatite. Analysis using FT-IR helps determine the presence of ap-

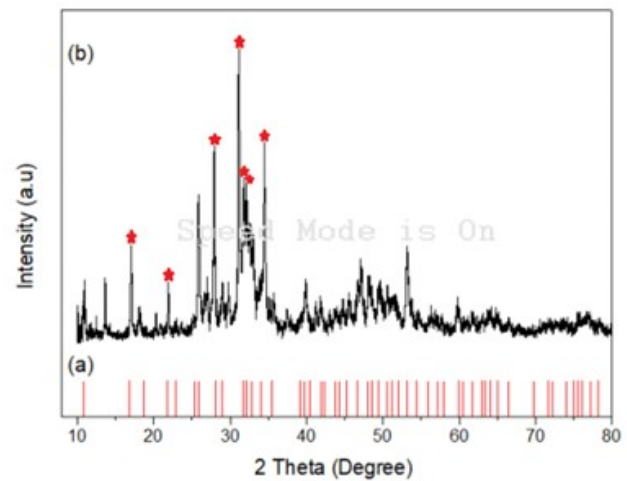


Figure 5. Diffractogram of (a) HAP Standard (JCPDS Number 09-0432) and (b) Hydroxyapatite

atite compounds defined by the existence of characteristic groups PO_4^{3-} . The spectrum of hydroxyapatite after and before absorption of Pb(II) metal ions is visible in Figure 6.

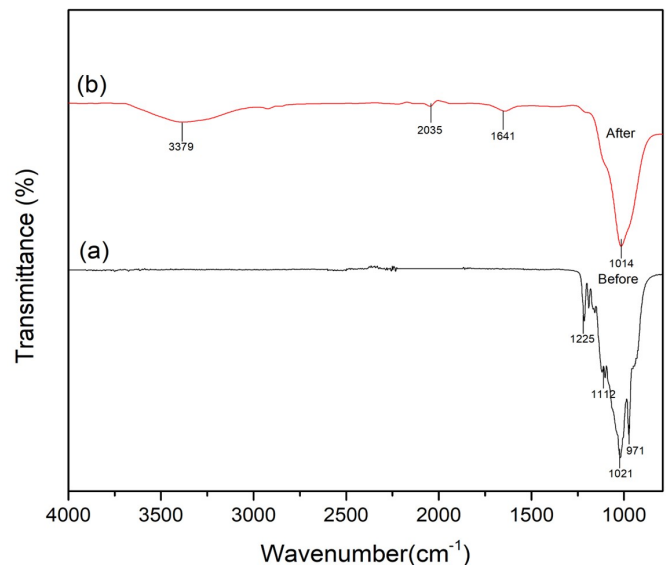
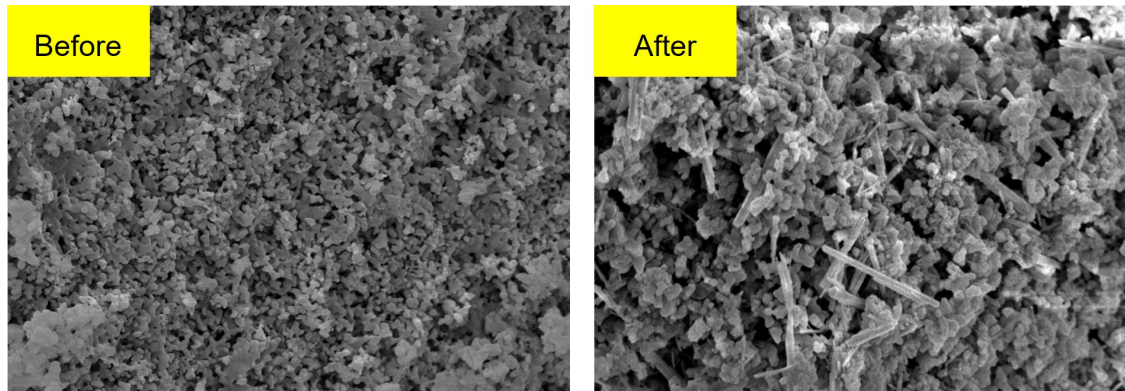


Figure 6. Spectra of Hydroxyapatite (a) Before and (b) After Pb(II) Metal Ion Absorption.

As shown in Figure 6, it is evident that there is a distinct alteration in the peaks before and after the uptake of Pb(II) ions, suggesting that functional groups like $-\text{OH}$, PO_4^{3-} , and CO_3^{2-} contribute to the adsorption mechanism (dos Santos Horta et al., 2020). The peak observed between 960 and 1100 cm^{-1} relates to the asymmetric stretching vibrations of PO_4^{3-} while the peak around 1225 cm^{-1} is also linked to these asymmetric stretching vibrations. Following

Table 2. Pseudo First Order and Pseudo Second Order Parameters for the Absorption of Pb(II) Metal Ions Using Hydroxyapatite

Parameters	Pseudo First Order			Pseudo Second Order		
	K_1 (min^{-1})	q_e (mg/g)	R^2	K_2 (min^{-1})	q_e (mg/g)	R^2
Pb(II)	-0.033	147.142	0.077	0.0050	1.0865	0.8221

**Figure 7.** Morphology of Hydroxyapatite Before and After Absorption

the adsorption the peak at 1641 cm^{-1} corresponds to the bending vibrations of H–O–H in bound water (H_2O), along with the way something looks the CO_3^{2-} peak at 2035 cm^{-1} and the O–H peak present at 3379 cm^{-1} . The surface characteristics of hydroxyapatite were analyzed using SEM-EDX under a magnification of 5000x. Figure 7 illustrates the morphological changes occurring after as well as the before adsorption of Pb(II).

Figure 7 reveals the SEM results of hydroxyapatite before and after adsorption. Before adsorption, the morphology of hydroxyapatite is agglomerated or clumped. Agglomeration is formed when small particles combine at high temperatures to form larger structures produced during the calcination process which causes the particles to coalesce and form agglomerates (Iconaru et al., 2018). After the adsorption of Pb(II) metal ions, there is a morphological change in hydroxyapatite, with the appearance of a large number of rod-shaped crystals indicating that Pb(II) metal ions were successfully absorbed by hydroxyapatite. EDX analysis aims to determine the elemental content and qualitative analysis of the Ca/P ratio in hydroxyapatite after as well as before adsorption of Pb(II) metal ions. The molar ratio obtained from hydroxyapatite was 1.72 (Table 3).

Table 3. Ca/P Ratio of Hydroxyapatite

Elements	Mass (%)	Ratio
Ca	31.36	1.72
P	18.23	

4. CONCLUSIONS

According to the findings, the levels of concentration, the mass of the adsorbent, and the duration of contact greatly affect the adsorption mechanism of Pb(II) ions when utilizing hydroxyapatite derived from quail eggshells. The best conditions for adsorption were established at a concentration of 800 mg/L , an adsorbent weight of 0.1 grams , as well as a contact period of 60 minutes , achieving an adsorption efficiency of Pb(II) ions at 71.48% , which corresponds with the Langmuir model and follows pseudo-second-order kinetics.

5. ACKNOWLEDGEMENT

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